APPENDIX

To the Amendment dated March 16, 2007 In reply to the Office Action of October 16, 2006 issued in

US APPLN SERIAL NO.: 10/783,866

DOCKET: TFH063

Chris Rauwendaal, Polymer Extrusion, Pg. 178
Hanser Publishers 1994 (4 pages)

Chris Rauwendaal

Polymer Extrusion





ion Molding

rization stics.

ı Molding ts

roperties neering in

xtrusion and

3

e Technologist,

ics Engineer

⊃olymer

itics Engineers,

Chris Rauwendaal

Polymer Extrusion



Third, revised edition



Hanser Publishers, Munich Vienna New York

Hanser/Gardner Publications, Inc., Cincinnati

Distributed in the USA and in Canada by Hanser/Gardner Publications, Inc. 6600 Clough Pike, Cincinnati, Ohio 45244-4090, USA Fax: +1 (5 13) 5.27-8950

Distributed in all other countries by Carl Hanser Verlag Postfach 860420, 81631 München, Germany Fax: +49(89)981264

The use of general descriptive names, trademarks, etc, in this publication, even if the former are not especially identified, is not to be taken as a sign that such names, as understood by the Trade Marks and Merchandise Marks Act, may according be used freely by anyone.

While the advice and Information in this book are betieved to be true and accurdate at the date of going to press, neither the authors nor the editions nor the publisher can accept any fegal responsibility for any errors or omissions: that may be made. The publisher makes no warranty, express or implied, with respect to the material contained herein.

Library of Congress Cataloging-in-Publication Data

Rauwendaal, Chris.

Polymer extrusion / Chris Rauwendaal. – 3rd, rev. ed. p. cm, includes bibliographical references and indexes. ISBN 1-66990-140-6 1. Plastic — Extrusion, I. Title.

1. Plastic -- Extrusion. TP 1175.E9R37 1994 668.4'13 -- dc20

94-29397

Die Deutsche Bibliothek -- CIP-Einheitsaufnahme

Rauwendaal, Chris:

Polymer extrusion / Chris Rauwendaal. – 3., rev. ed. – Munich; Vienna; New York: Hanser, 1994

ISBN 3-446-17960-7 (Munich...) ISBN 1-56990-140-6 (New York)

All rights reserved. No part of this book may be reproduced or transmitted in any or by any means, electronic or mechanical, including photocopying, recording or by any information storage and retrieval system, without permission from the publisher.

Copyright © Carl Hanser Verlag, Munich Vienna New York 1994 Printed in Germany by Druckerel Appl, Wernding Plug flow generally does not happen in polymer melts, except in the case of wall slip (PVC). However, it does occur with granular polymeric solids. The solids conveying theory of single screw extruders is based on the assumption of plug flow of the solid polymer.

SHEAR RATE (γ): The difference in velocity per unit normal distance (normal to the direction of flow).

The rate of shearing or shear rate is one of the most important parameters in polymer melt processing. If the process is to be described quantitively, the shear rate in the fluid at any location needs to be known. The shear rate is generally written with the Greek letter gamma, $\hat{\gamma}$, with the dot above the gamma indicating a time derivative $\left(\hat{\gamma} = \frac{d\hat{\gamma}}{dt}\right)$. In terms of Figure 6—8, the shear rate can be written as:

$$\dot{\gamma}_{AB} = \frac{v_A - v_B}{AB} \tag{6-10}$$

Equation 6-10 is only valid for very small values of the normal distance AB. More accurately, the shear rate is:

$$\hat{\gamma}_{AB} = \lim_{AB \rightarrow 0} \frac{v_A - v_B}{AB} = \frac{dv(x)}{dy} \tag{6-11}$$

From equation 6-11, it can be seen that the local shear rate equals the local gradient of the velocity profile. Thus, if the velocity profile is known, the shear rate at any location can be determined.

SHEAR STRAIN (7): Displacement (in the direction of flow) per unit normal distance over a certain time period.

The shear strain is generally written with the Greek letter gamma (γ) , this time without the dot! The relationship between shear rate $(\dot{\gamma})$ and shear strain (γ) is:

$$\dot{\gamma} = \frac{d\gamma}{dt}$$
 and $\gamma = \int \dot{\gamma} dt$ (6-12)

In terms of Figure 6-8, the shear strain can be written as:

$$\gamma_{AB} = \frac{x_A - x_B}{AB} = \frac{\Delta x}{\Delta y} |_{AB} = \tan \beta \qquad (6-13)$$

The units of shear rate are \sec^{-1} and the shear strain is a dimensionless number.

SHEAR STRESS (t): The stress required to achieve a shearing type of deformation.

When a fluid is sheared, a certain force will be required to bring about that deformation. This force divided by the area over which it works is the shear stress. The shear stress is generally written with the Greek letter tau (t). In a simple example, shown in Figure 6-10, the shear stress is: Figure 6-10. Simple Shear De

$$\tau = \frac{F}{A}$$

and the shear rate is:

$$\dot{\gamma} = \frac{v}{\Delta}$$

SHEAR VISCOSITY (n):

$$\eta = \frac{\tau}{\hat{\gamma}}$$

The shear viscosity is gene stress x time. The viscosity Poise). In order to determ rate in a certain shear defe are available to determine ters.

NEWTONIAN FLUID:

Most low viscosity liquidversus shear rate, a Newto b. Therefore, Newtonian i A plot of shear stress vers

NON-NEWTONIAN FL

High viscosity polymer n with increasing shear rate Another type of non-Nev creases with increasing s

Figure 6-11. Flow Curves tonian Fluid, and a Pseudo